Biomass Gasification

- Chemical process in which any carbonaceous (solid or liquid) fuel is converted to gaseous fuel.
- Involves partial combustion of biomass.
- Product gases can be used to produce heat and energy and also fuels.

• Product gas: H₂, H₂O, CO, CO₂, CH₄, N₂ and impurities e.g. ash, tars, H₂S, HCl and alkali species.



Biomass Gasification

• Chemical process in which any carbonaceous (solid or liquid) fuel is

Any problem in the gasification process?

The presence of corrosive species dictates the boundaries within which, e.g., superheaters and syngas coolers will operate.

tars, H₂S, HCl and alkali species.

Corrosion studies in biomass/waste gasification is scarce!

Thus...

It is of great importance to increase our knowledge about this complex corrosion process.





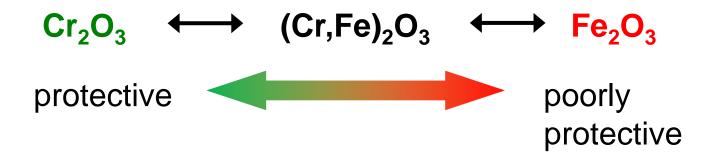
Exposure Matrix:

Samples: Stainless steel (304L) and low alloyed steel (T22)

- Temperature: 600 °C
- Time: 4 hours
- Complex environment: H₂, H₂O, CO, CO₂, HCl, H₂S, KCl, etc

The properties of the protective oxide formed on FeCr alloys

The oxide formed on FeCr alloys consist of a corundum type solid solution, $(Cr, Fe)_2O_3$. The Cr/Fe ratio determines whether it is protective (as Cr_2O_3) or poorly protective (as Fe_2O_3).



However, the oxygen activity in an gasifier environment is typically in the order 10⁻²⁵. At 600 °C, Fe₂O₃ is not stable in this environment!



Hence, reactions that deplete the oxide in chromia tend to destroy the protective properties of the oxide!

$$(Cr, Fe)_2O_3$$
 $O_2 + H_2O(g)$ $Fe_2O_3 + CrO_2(OH)_2(g)$

$$O_2 + H_2O$$

 $p_{eq}(CrO_2(OH)_2): 0.15ppm$

(600°C, *p*O₂: 0.6bar, *p*H₂O: 0.40bar)

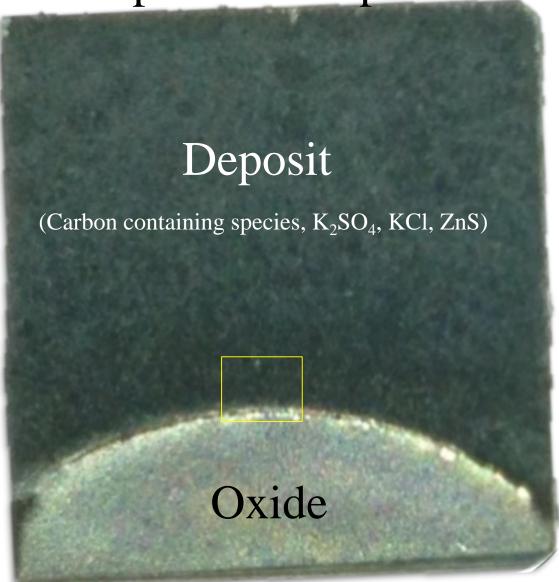
$$Cr_2O_3(s) + 2H_2O(g) + 1.5O_2(g) \rightarrow 2CrO_2(OH)_2(g)$$

Oxygen is needed!





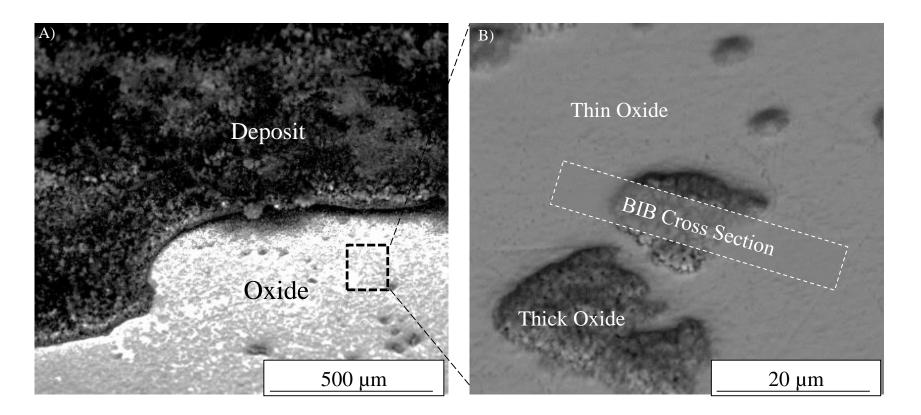
Sample After exposure





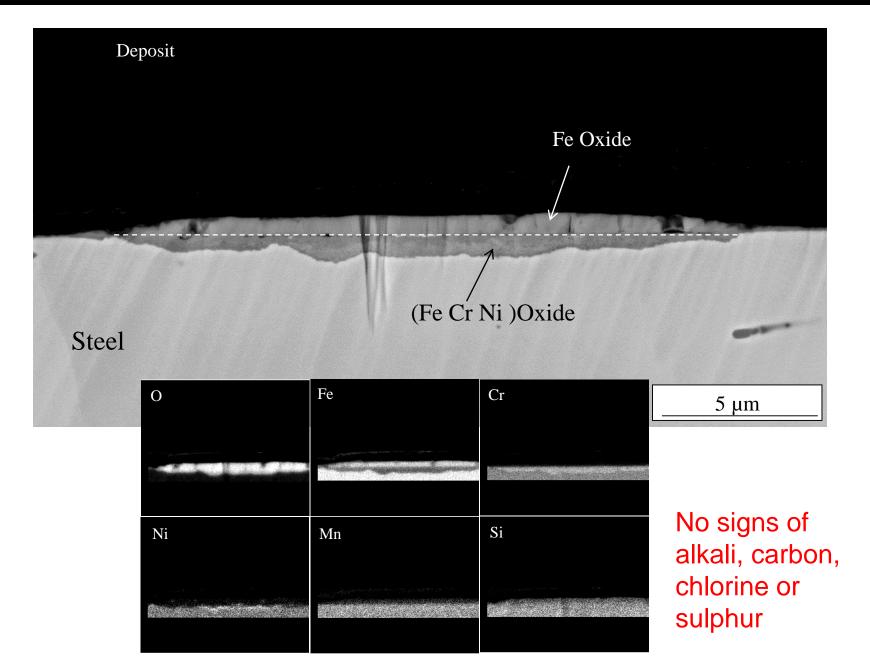


304L exposed for 4 hours at 600 $^{\circ}$ C in the Chalmers gasifier

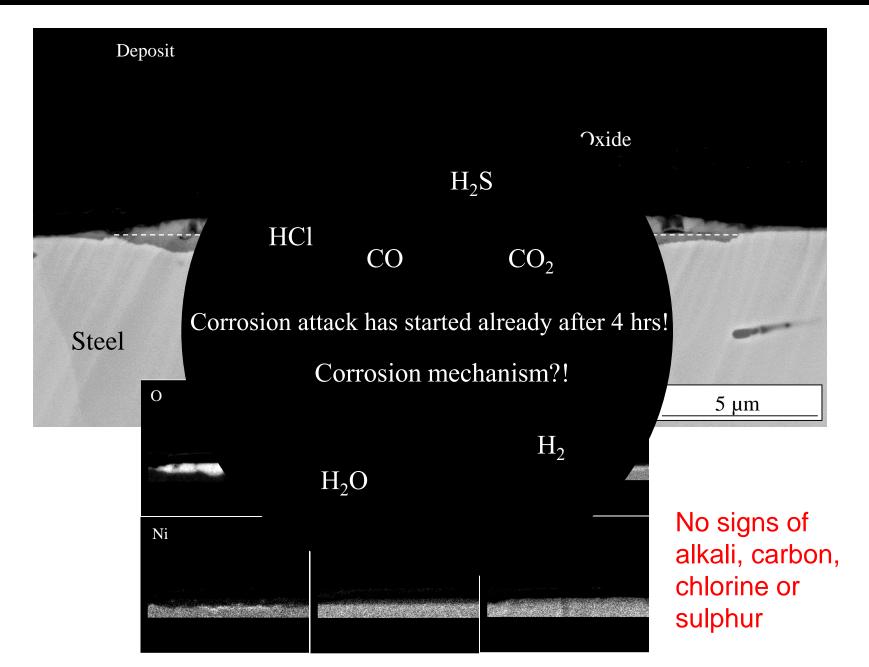


304L (bal% Fe,18% Cr, 10% Ni, 0.1% Mn)







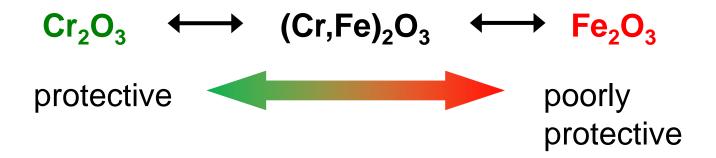






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However, the oxygen activity in an gasifier environment is typically in the order 10⁻²⁵. At 600 °C, Fe₂O₃ is not stable in this environment!



Laboratory Studies

Focusing on H₂-H₂O environments

Composition [wt%]	Cr	Мо	С	Mn	Si	Minor Add.	Fe	Ni
304L(18/8)	18.18	0.53	0.022	1.53	0.31	Present	Bal.	8.10

Dry oxygen/air

Cr-rich $(Fe_xCr_{1-x})_2O_3$

Protective



Humid oxygen/air

Cr-depleted $(Fe_xCr_{1-x})_2O_3$ Non-protective

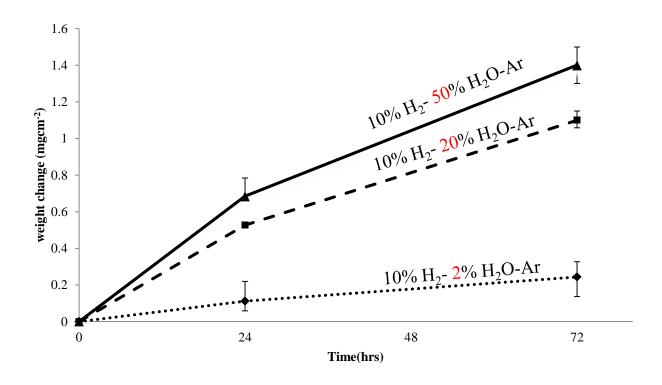


 H_2 - H_2O





Laboratory exposures in low pO_2

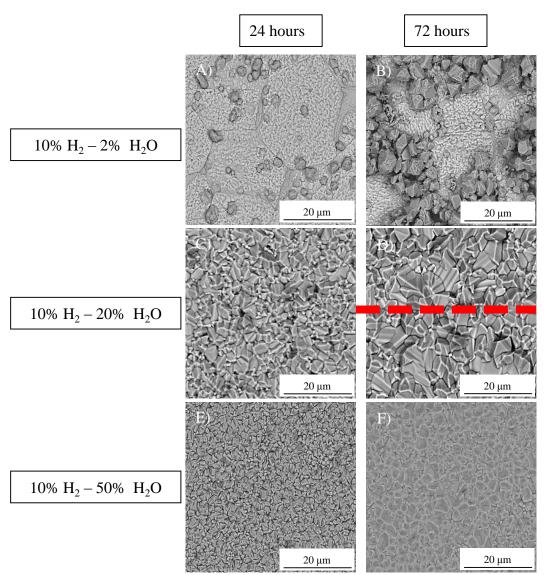


Exposure	H ₂ (volume %)	H ₂ O (volume %)	Calculated a(O ₂)
1	10	2	5*10 ⁻²⁶
2	10	20	5*10 ⁻²⁴
3	10	50	3*10-23

• 304L exposed to 10% H_2 - X% H_2 O-Ar at 600 °C for 24 and 72 hours.



Laboratory exposures in low pO_2

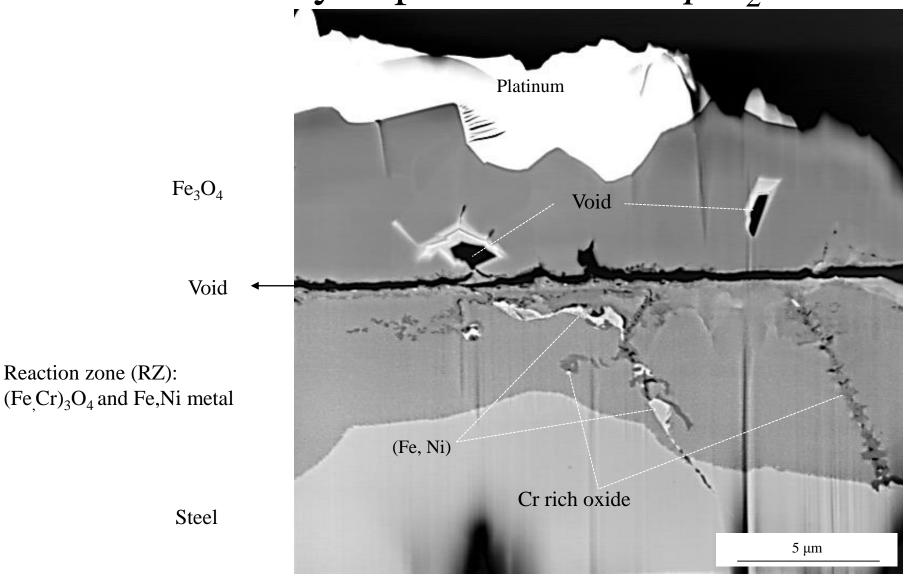


Cross section



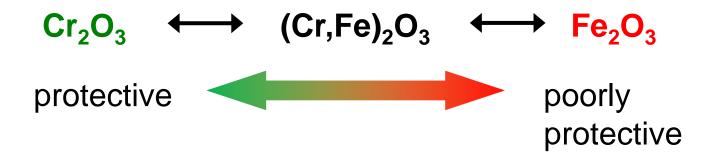


Laboratory exposures in low pO_2

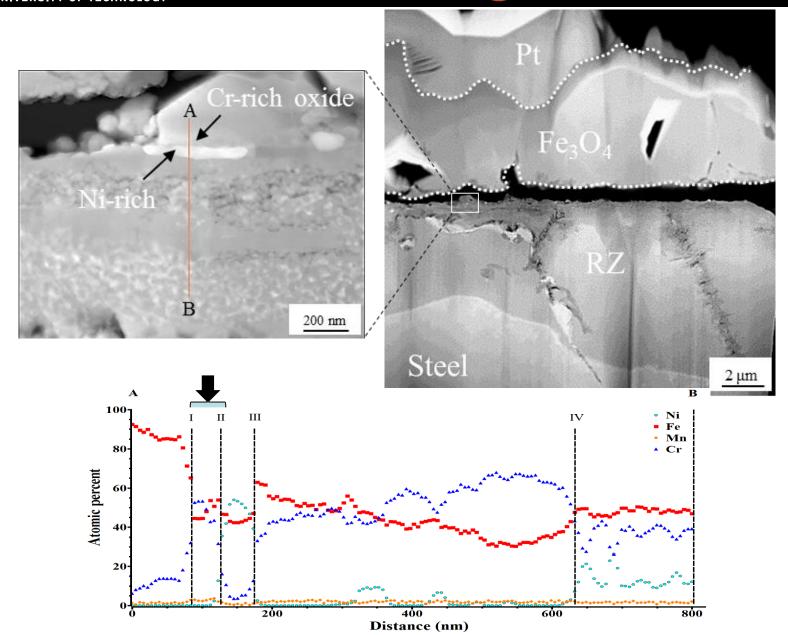


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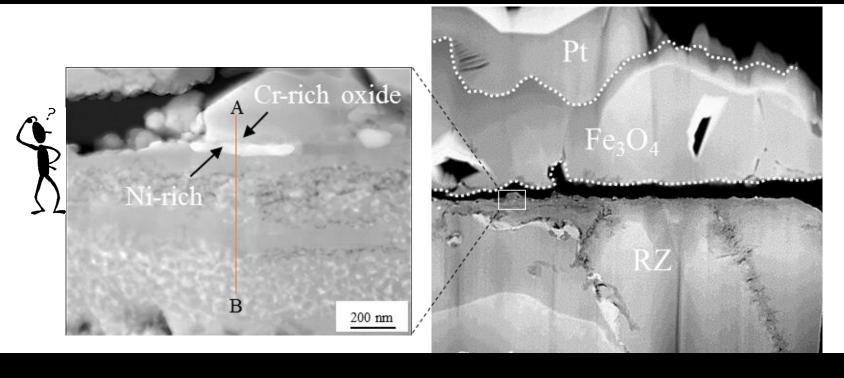
However, the oxygen activity in an gasifier environment is typically in the order 10⁻²⁵. At 600 °C, Fe₂O₃ is not stable in this environment!



STEM/HAADF cross section image of 304L exposed to 10 % H₂- 20% H₂O-Ar at 600 °C for **72 hours.**







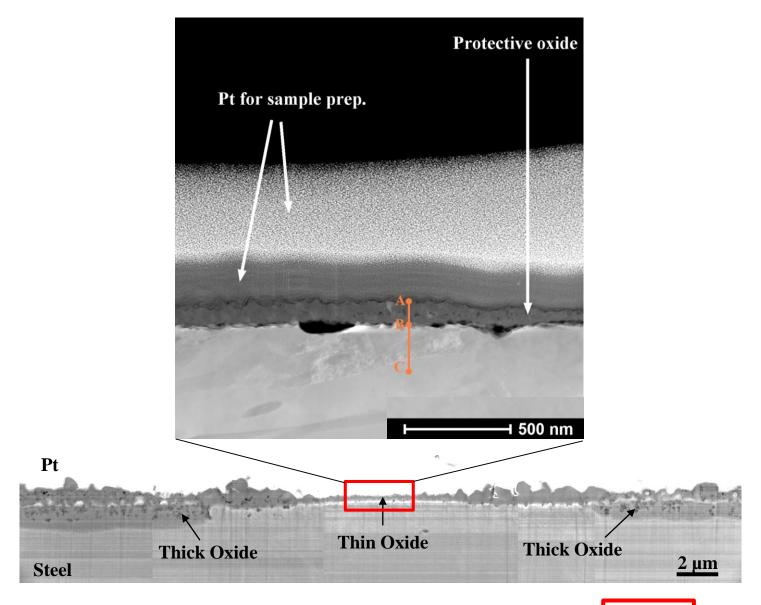
Is it the remnant of initially formed Cr-rich oxide?

Need to perform a shorter exposure!

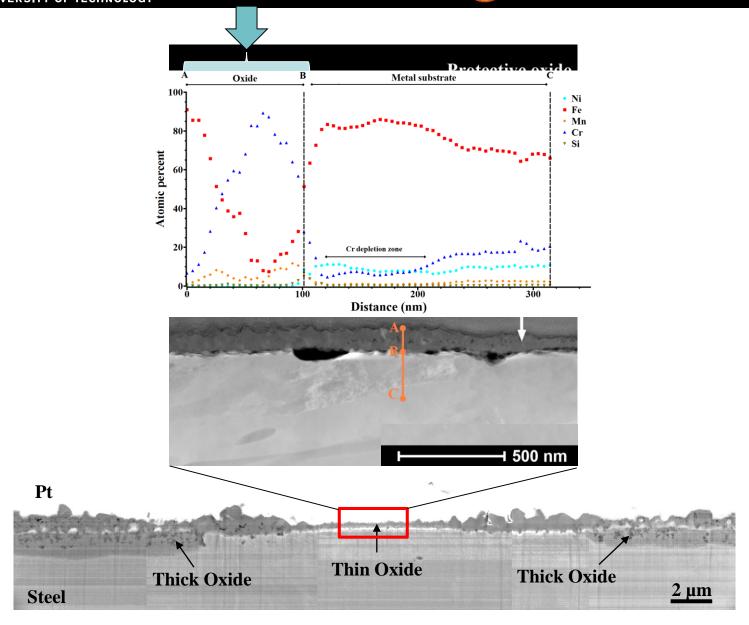
• STEM/HAADF cross section image of 304L exposed to 10 % H₂- 20% H₂O-Ar at 600 °C for **72 hours.**







STEM/BSE image of 304L exposed to 10 % H₂- 20% H₂O-Ar at 600 °C for **1 hour.**



STEM/BSE image of 304L exposed to 10 % H₂- 20% H₂O-Ar at 600 °C for **1 hour.**



Cr evaporation in presence of H_2O at **high** $a(O_2)$ But

Negligible at low $a(O_2)$!

Dry oxygen/air

Cr-rich $(Fe_xCr_{1-x})_2O_3$

Protective



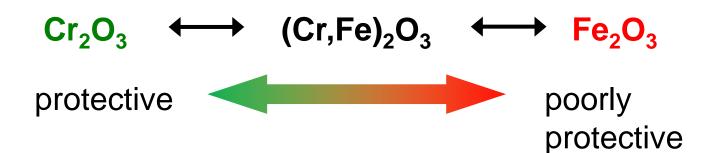




Cr-rich (Fe_xCr_{1-x})₂O₃

Non-protective







Cr evaporation in presence of H_2O at **high** $a(O_2)$ But

We are missing something...

$$Cr_2O_3 \longleftrightarrow (Cr,Fe)_2O_3 \longleftrightarrow Fe_2O_3$$
protective poorly protective

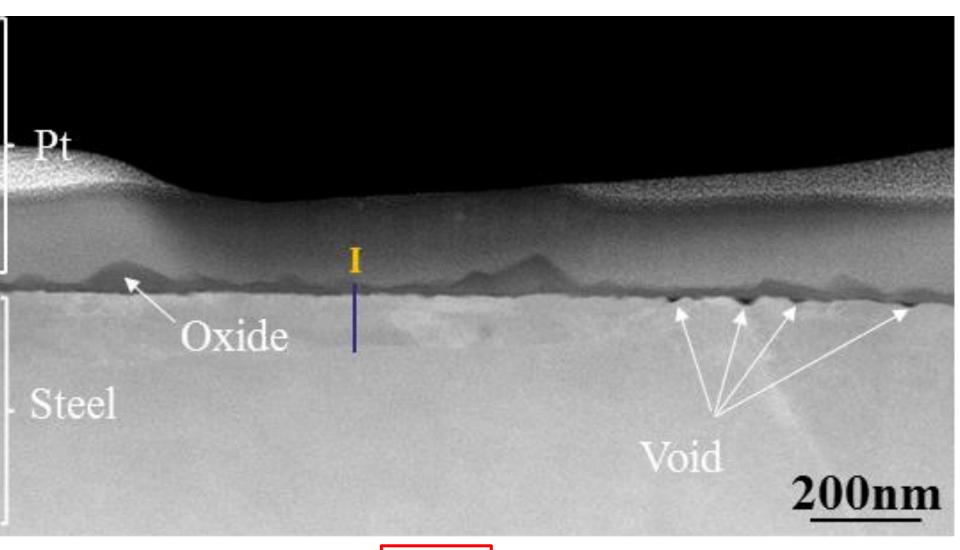




Dry oxygen/air

Cr-rich $(Fe_xCr_{1-x})_2O_3$

Protective

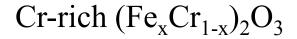


• STEM/BSE image of 304L exposed to 5 % O₂- N₂ at 600 °C for 24 hour.

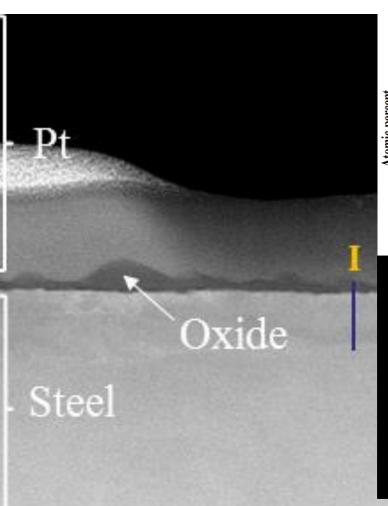


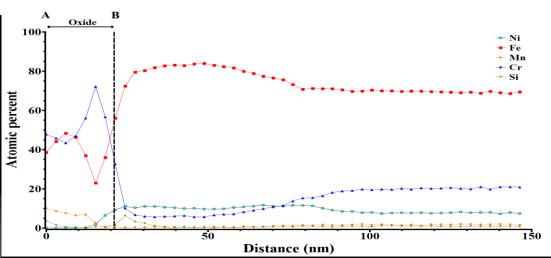


Dry oxygen/air



Protective





Cr-rich Oxide

Oxide thickness: $\approx 10 \text{ nm}$

Cr level (oxide): $\approx 70 \text{ cat.}\%$

Alloy

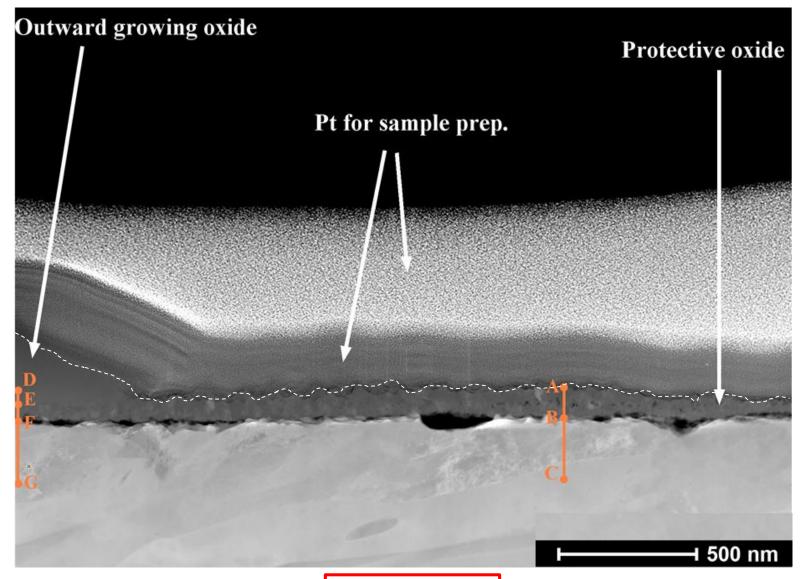
Cr level in depletion zone: ≈ 6 atm.%





 H_2 - H_2O

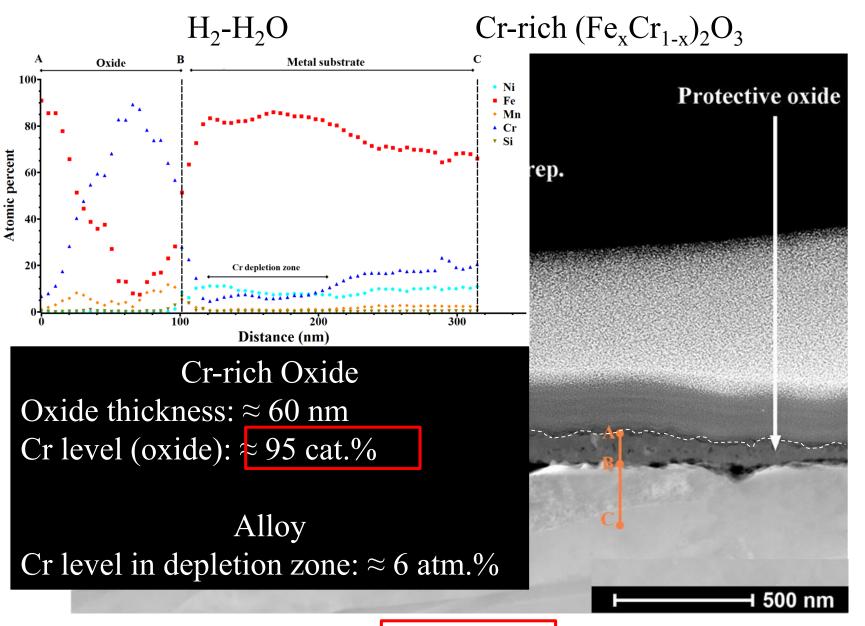
Cr-rich (Fe_xCr_{1-x})₂O₃



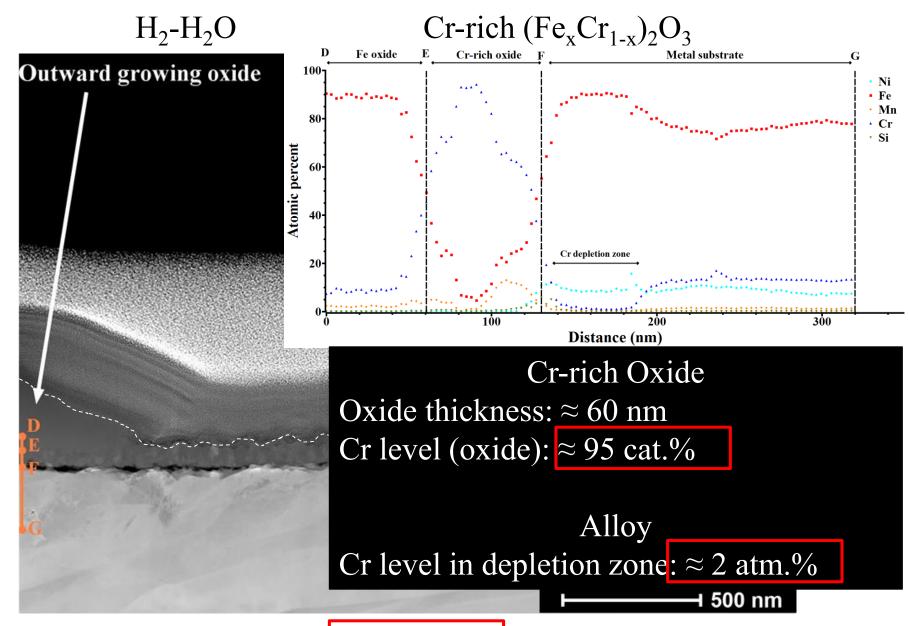
• STEM/BSE image of 304L exposed to 10 % H₂- 20% H₂O at 600 °C for 1 hour.







STEM/BSE image of 304L exposed to 10 % H₂- 20% H₂O at 600 °C for 1 hour.



STEM/BSE image of 304L exposed to 10 % H₂- 20% H₂O at 600 °C for 1 hour.





H₂-H₂O compare to dry oxygen:

- The base oxide is almost pure chromia.

Faster oxidation rate than $(Fe_xCr_{1-x})_2O_3$

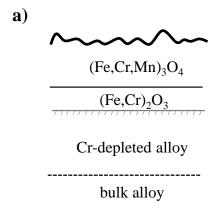
- The base oxide is thicker.
- Significant Cr-depletion zone exists at the oxide/alloy interface.

This can describe the breakaway oxidation mechanism!





Exposing to $O_2 + N_2$ at 600 °C







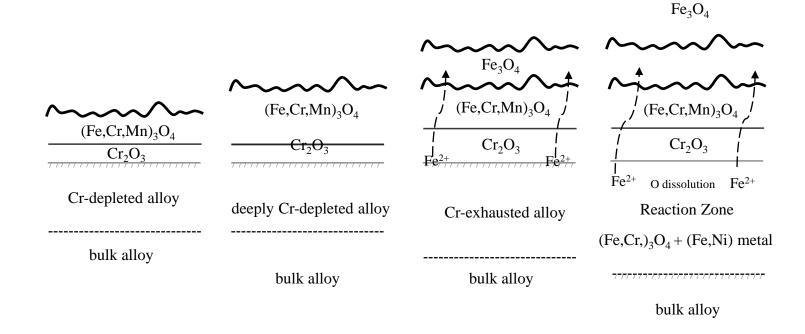
Exposing to H_2 - H_2O at 600 °C

b) Stage I

c) Stage II

d) Stage III

e) Stage IV





Perfect!

Now we have the breakaway oxidation mechanism!

But

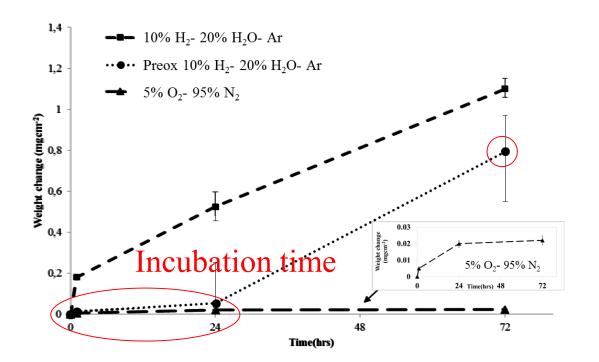
The last puzzle of the mechanism: why do we form pure chromia, instead of $(Fe_xCr_{1-x})_2O_3$, in H_2 - H_2O ?





If sample is pre-oxidized in $O_2 + N_2$ first i.e. forming Cr-rich (Fe_xCr_{1-X})₂O₃

then exposed to H_2 - H_2 O

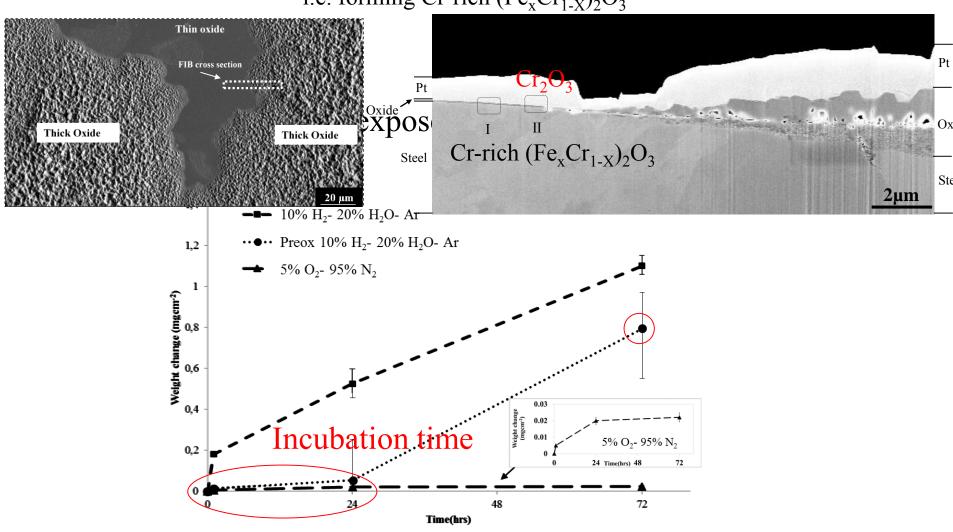






If sample is pre-oxidized in $O_2 + N_2$ first

i.e. forming Cr-rich (Fe_xCr_{1-X})₂O₃



Three main points:

• When as-polished sample exposed to H₂-H₂O

 Cr_2O_3

• When pre-oxidized sample exposed to H₂-H₂O

 $(Fe_xCr_{1-x})_2O_3$

Replaced by

 Cr_2O_3



Incubation time for pre-oxidized sample before breakaway oxidation

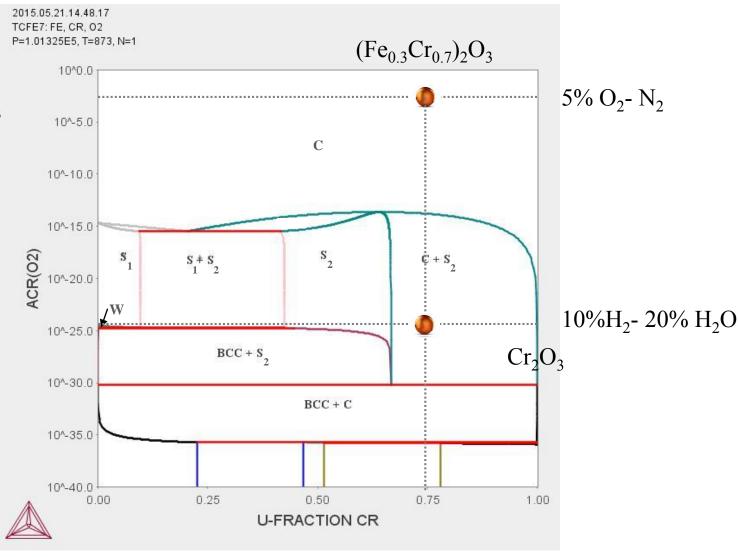
 $C = corundum-type M_2O_3$

$$S_1 = Fe_{3-x}Cr_xO_4$$

$$S_2 = FeCr_{2-x}Fe_xO_4$$

$$W = Fe_{1-x}O$$

BCC = ferrite-structured metal

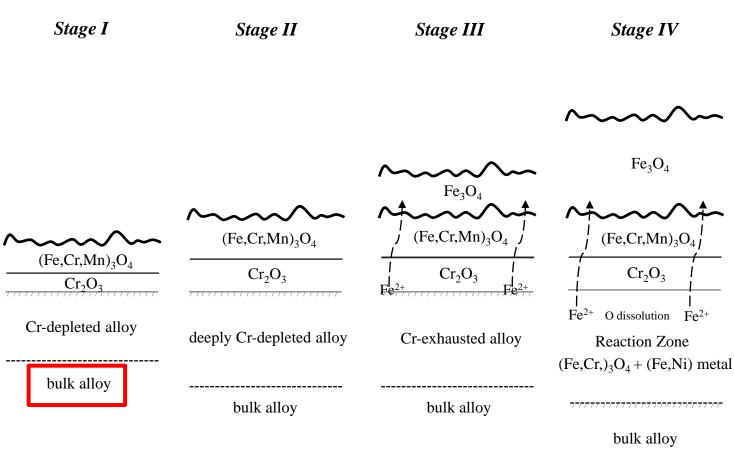


Stable phases in the Fe-Cr-O system at 600 °C as a function of oxygen activity and mole fraction of Cr calculated using the THERMO-CALC.





Breakaway oxidation in H₂-H₂O at 600 °C



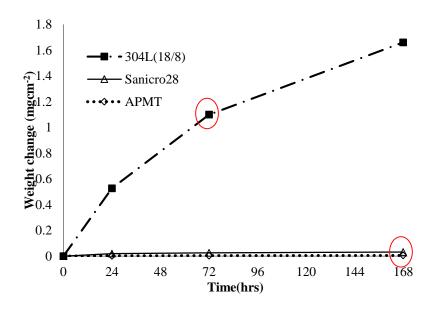
What if the alloy has enough Cr-reservoir?





Mitigate corrosion by improved materials

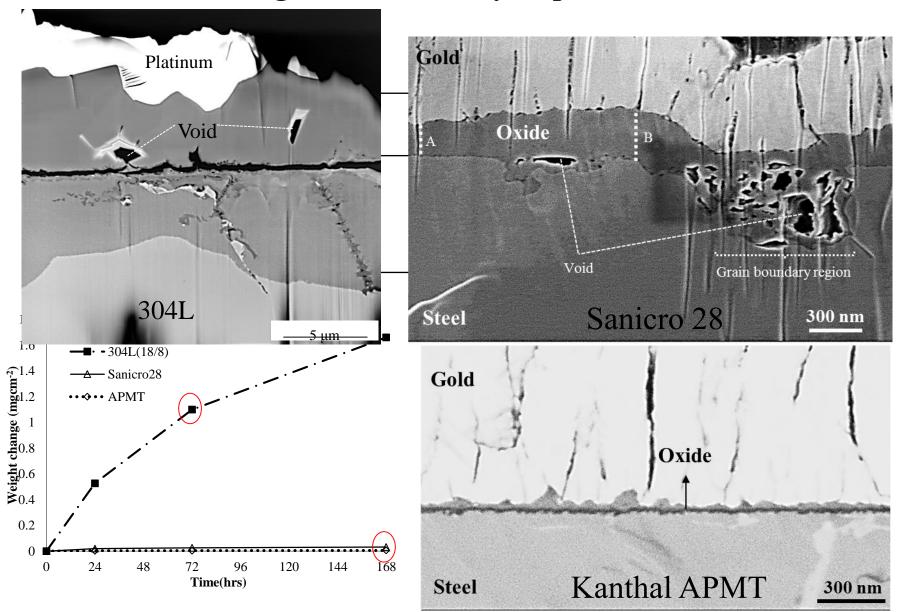
Composition [wt%]	Cr	Al	Мо	C	Mn	Si	Minor Add.	Fe	Ni
304L(18/8)	18.18	-	0.53	0.022	1.53	0.31	Present	Bal.	8.10
Sanicro 28	27	_	3.5	0.02	2	0.7	Cu	Bal.	31
Kanthal APMT	22	5	3	≤0.05	≤0.4	≤0.7	Present	Bal.	-







Mitigate corrosion by improved materials

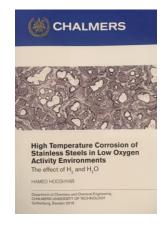


Summary

- Low oxygen activity environments can cause (marginal) chromia forming steels to go into breakaway oxidation
 - This is due to a Cr exhausted alloy beneath the oxide leading to iron oxidation
- More highly alloyed stainless steels and alumina formers exhibit more protective behaviour in this environment.
- Important to point out that this has been a fundamental study focusing on the corrosion mechanism in low oxygen activity environment containing H₂ and H₂O



CO, CO₂, CH₄, H₂S, HCI, KCI etc may still cause corrosion!!



Hamed Hooshyar Doctoral Thesis Defense

Friday 18 March at 13.00 at Chalmers

"High Temperature Corrosion of Stainless Steels in Low Oxygen Activity Environments -The effect of H₂ and H₂O"

- **Paper I** Field study in Chalmers Gasifier
- **Paper II** Process investigation
- **Paper III** General effects of H_2 and H_2O
- **Paper IV** Mechanistic study of corrosion in presence of H_2O at low $a(O_2)$
- **Paper V** Propagation after breakaway oxidation
- Paper VI Oxidation behavior of other alloys
- **Paper VII** Influence of $a(O_2)$ on the base oxide